Mixed transition metal oxides for efficient electrochemical splitting of water to hydrogen and oxygen

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Abstract

In this study non-noble and non-rare metal based mixed transition metal oxides were synthesized by spray pyrolysis and used as electrocatalysts for the efficient splitting of water to hydrogen and oxygen in alkaline medium. The mixed oxides of nickel and cobalt (Ni-Co-oxide) of specific compositions (3:1 ratio) generated the much smaller Tafel slopes (210 mV decade\(^{-1}\)) compared to 330 mVdecade\(^{-1}\) and 440 mV decade\(^{-1}\) for Co-Oxide and Ni-oxide respectively indicating its enhanced electro-catalytic activity for oxygen evolution reaction (OER) during water splitting. Also, the mixed oxides of Ni and Fe (Ni-Fe-oxide) of specific compositions (4:1 ratio) generated the smaller Tafel slopes (360 mV decade\(^{-1}\)) compared to 440 mVdecade\(^{-1}\) and 500 mV decade\(^{-1}\) for Ni-oxide and Fe-oxide respectively for OER during water splitting. At the measured potential of 1.0 V/SCE the current density of 130.0 mA cm\(^{-2}\) was observed for water splitting at Ni-Co mixed oxide compared to 60.0 mA cm\(^{-2}\), 31.0 mA cm\(^{-2}\), 30.0 mA cm\(^{-2}\) and 28.0 mA cm\(^{-2}\) at mixed Ni-Fe oxide (4:1 ratio), Co-oxide, Ni-Oxide and Fe-oxide respectively. These results show more than four-fold increase in rate of water splitting at the mixed Ni-Co oxide and more than two-fold at mixed Ni-Fe oxide due to synergetic effects compared to their individual oxides. An order of magnitude of higher values of current density for water splitting on these electrodes compared to recently reported results can be attributed also to high internal surface area due to porosity of the oxide films synthesized by spray pyrolysis method as it is observed in SEM results.

Keywords: mixed transition metal oxides, electrocatalytic anodes, water splitting, water oxidation, porous films, oxygen evolution.
1 Introduction

Water splitting reaction to produce hydrogen and oxygen is a well-known electrochemical process. It requires an external applied potential to overcome the thermodynamic, ohmic and kinetic barriers to drive water-splitting reaction. Pollution free hydrogen fuel generation and the flexibility of choosing the external power sources such as electrical grid or solar cell [1] have made water electrolysis the most desirable compared to traditional processes that use fossil fuels as hydrogen source. The abundant and cost effective solar energy can be used to generate the external power required to drive the electrolysis reaction. However, the present water electrolyzer’s low current efficiency has made the process less competitive compared to steam reforming methanol or natural gas [2]. Most of the research efforts to improve the water electrolysis efficiency have been focusing on the energetically challenging water oxidation to generate oxygen at anodes and thereby facilitate hydrogen evolution reaction (HER) at cathodes during water splitting reactions ($\text{H}_2\text{O} \rightarrow \text{H}_2 + \frac{1}{2} \text{O}_2$). Earlier work included noble metals and rare metal oxides such as RuO$_2$ or IrO$_2$ for oxygen evolution reaction (OER). However, the dependence on rare metals is not a solid approach because a massive worldwide manufacturing of noble/rare metal-based electrolysers will drive up their price further. Perhaps the most suitable approach is to use earth abundant transition metals and their oxides or a combination of transition metals and their oxides to quell the overpotential required for oxygen evolution at the anode surface. Ni, Co and their oxides have been extensively studied individually or as alloys as electrocatalytic electrodes for the oxygen evolution reaction [3–12]. Previous investigations on transition metals M-single oxides (M = Ni, Co or Fe) were focused on enhancing the catalytic activity for OER by modifying the surface morphologies and studying their behavior during OER. However, the extent to which the catalytic activity of these transition metal single oxides toward OER can be enhanced was found to be rather limited. The other available alternative to use earth abundant transition metal based electrodes for OER is the mixed first row transition metal oxides. The synergetic effects of the later on electrocatalytic activities were recognized earlier [13–20]. The effect of methods of synthesis of these mixed oxides electrodes and their composition on electro-catalytic activity for OER were also noted [12].

In this study mixed Ni-Co-oxides, mixed Ni-Fe oxides with different atomic ratios, individual Ni-oxide, Co-oxide and Fe-oxides were synthesized by spray pyrolysis method on conducting fluorine doped tin oxide (FTO) coated glass substrate. The electrocatalytic activity of the mixed Ni-Co-oxide and Ni-Fe oxide anodes for oxygen evolution in basic medium was assessed in terms of current density and compared to those of individual oxides. The surface morphology and composition of these oxide electrodes were characterized using the scanning electron microscopy (SEM) and energy dispersive spectroscopy (EDS) respectively.
2 Experimental

Commercially available fluorine doped tin oxide (FTO) coated conducting glass substrates were cleaned in a sonicator using acetone, Acetone: Di-water (50:50) and Di-water respectively. Each step lasted 30 minutes. The cleaned FTO glass substrates were then dried under dry Argon gas. The resistivity of the resulting ITOs was found to be within 14–20 ohm cm at room temperature. Aqueous solutions of 0.05 M Ni-Chloride, 0.05 M Co-nitrate and 0.05 M Fe-Nitrate were used as spray solutions to synthesize Ni-oxide, Co-oxide and Fe-oxide respectively. Different volume ratios of these aqueous solutions were also used to synthesize mixed Ni-Co oxides and mixed Ni-Fe oxides. The spray operation was carried out for a total of 30 sec having three 10 sec spray periods on an FTO conducting glass substrate at a temperature of 180ºC using a pneumatic nozzle and oxygen as the carrier gas with a pressure of 137.8 kPa. In between each spray period there were intervals of ~ 10 min for the substrate temperature to be raised back to 180ºC on a hot plate. A conducting silver epoxy was applied to the four edges of the FTO glass to ensure a uniform electrical conductivity across the electrode surface area during water electrolysis. After the spray the silver epoxy at the edges of the electrodes was covered with a non-conductive resin based epoxy. Linear sweep voltammetry was used as the main tool to assess the electrocatalytic performance of these electrodes toward OER. A three-electrode configuration in a single-compartment cell was used, with Ni-Co mixed oxides, Ni-Fe mixed oxide, Ni-oxide, Co-oxide or Fe-oxide as a working electrode, platinum wire as a counter electrode, and SCE as a reference electrode. The single compartment cell was filled with 2.5 M KOH as an electrolyte solution. The linear sweep CV curves of the catalysts were obtained using a scanning potentiostat (Versa STAT 3 running Versa Studio software, Princeton Applied Research). A scan rate of 50 mV s⁻¹ was used to minimize the extra resistances developed at the electrode-solution interfaces by the bubbles of oxygen and hydrogen generated during water splitting reactions.

Scanning electron microscopy (SEM) was used to characterize the surface morphology of these synthesized thin films and was performed on a high-resolution Hitachi S-3400 SEM using a 2.0 kV focus voltage. The Hitachi S-3400 SEM equipped with a Bruker Quantax energy dispersive spectrometer was also used for EDS analysis. Samples were mounted on a double-sided carbon tape affixed to an Aluminum specimen holder. The EDS spectra were collected at a working distance of 10 mm and an accelerating voltage of 15 KV.

3 Results and discussion

Figure 1(a) shows the current density versus the external applied potential curves for mixed Ni-Co oxide, Ni-oxide, Co-oxide, Fe-oxide and bare FTO during OER. In this Figure the mixed Ni-Co oxide (synthesized using 3:1 volume ratio of 0.05 M NiCl₂ and 0.05 M Co(NO₃)₂ in spray solution and sprayed for total of 30 sec) catalyst showed the highest and bare FTO showed the lowest electrocatalytic
Figure 1: Current density, $J$ (mA cm$^{-2}$) versus applied potential ($E$, V/SCE) during OER (a) at bare FTO conducting glass, Ni-oxide, Co-oxide, Fe-oxide and mixed Ni-Co-oxide electrodes (b) at mixed Ni-Co-oxides of various compositions deposited on FTO coated glass substrate (c) at mixed Ni-Fe oxides of various compositions in 2.5 M KOH solution at a scan rate of 50 mV s$^{-1}$. 
activity toward OER during water splitting. The observed sharp rise in current
density for OER at Ni-Co-mixed oxides at 0.7 V/SCE compared to those at the
individual Ni and Co oxides indicates that the presence of Co along with Ni
generates active mixed oxide surfaces having lower overpotential for OER. For
example, at 1.0 V/SCE the observed current density of 130.0 mA cm$^{-2}$ at mixed
Ni-Co-oxide is over 4-fold higher compared to observed current density of $\sim$ 30.0
mA cm$^{-2}$ on their individual oxides. Similarly, at 1.0 V/SCE the observed current
density of 60.00 mA cm$^{-2}$ at mixed Ni-Fe oxide (synthesized using 4:1 volume
ratio of 0.05 M NiCl$_2$ and 0.05 M Fe(NO$_3$)$_3$ in spray solution and sprayed for total
of 30 sec) is over 2-fold higher compared to observe current density of 28.00 mA
cm$^{-2}$ on Fe-oxide itself (see Figures 1(a) and 1(c)).

The observed broad peaks prior to oxygen evolution in Figure 1(b) clearly
indicates the existence of direct relationship between the position of these peaks
and an early oxygen evolution. In the case of mixed Ni-Co-oxide electrodes of 3:1
ratio shows the formation of electro-chromic Ni-oxide at lower potential compared
to other compositions [21]. Consequently, mixed Ni-Co oxide of 3:1 ratios shows
the highest synergetic electrocatalytic effect towards OER. However, in Figure
1(c) no clear broad peaks are observed for mixed Ni-Fe oxides of various
composition. In this case the mixed oxide having Ni:Fe ratio of 4:1 shows highest
electrocatalytic effect towards OER during water splitting. However, the
synergetic effect between nickel and iron towards electrocatalysis of OER is lower
than that of nickel and cobalt. But cost wise iron will be lower in cost than cobalt
to offset its lower synergetic electrocatalytic effect compared to cobalt.

Figure 2 shows the Tafel plots of these five metal oxides. The mixed Ni-Co
oxide anode sprayed pyrolytically on FTO exhibits the lowest Tafel slope of 210
mV/decade compared to 330 mV/decade for Co-oxide and 440 mV decade$^{-1}$ for
Ni-oxide anodes for OER, 360 mV decade$^{-1}$ for mixed Ni-Fe oxide and 500 mV
decade$^{-1}$ for Fe-oxide anodes for OER during water splitting. The lowest Tafel
slope for mixed Ni-Co oxide and mixed Ni-Fe oxide compared to their individual
oxides indicated their higher electrocatalytic activity due to synergetic effect
[13, 14] of mixed oxides that generated active surface sites for efficient OER.

The surface morphologies and the corresponding compositions were obtained
from the scanning electron microgram (SEM) pictures and the corresponding
energy dispersive spectroscopic (EDS) data given in Figure 3 for Co-oxide, Ni-
oxide and mixed Ni-Co-oxides respectively. The microgram in Figure 3 clearly
indicates the rough and porous surface of Co-oxide and the corresponding EDS
data shows the presence of Co, O and Sn on the surface as expected. Similarly, the
microgram in Figure 3 shows a less rough surface of Ni oxide and the
corresponding EDS data showed the presence of Ni, O and Sn. The microgram of
mixed Ni-Co oxide (Figure 3) shows the roughest and most porous surface. The
corresponding EDS data shows the presence of Ni, Co, Sn and O as expected.
These rough and porous surfaces are responsible for the enhanced internal surface
area that helped to generate an order of magnitude higher current densities
compared to recently reported results [15–19]. The internal surface area for the
rough and porous surface could be $\sim$ 10$^4$ times higher than the geometrical surface
area [16].
Figure 2: Tafel plots obtained from the Log (current density, J) vs overpotential, $\eta$) for OER at mixed Ni-Co oxide, mixed Ni-Fe oxide, Ni-oxide, Co-oxide and Fe-oxide electrodes. The overpotentials for OER were obtained using $\eta = E_{\text{meas}} - E^0_{\text{OER}}$ where $E^0_{\text{OER}} = 0.116$ V/SCE is the standard oxygen evolution potential in 2.5 KOH electrolyte and $E_{\text{meas}}$ is the measured potential during OER.

Figure 3: SEM pictures and EDS results of Co-oxide, Ni-oxide and mixed Ni-Co mixed oxide on FTO coated glass substrate.
4 Conclusions

Electrocatalytically active porous with high internal surface area Ni-oxide, Co-oxide, Fe-oxide, mixed Ni-Co-oxide and mixed Ni-Fe oxide anodes can be synthesized by spray pyrolysis method on fluorine doped tin oxide (FTO) coated glass substrate. The synergetic effect of mixed oxides helped to generate more active electrocatalytic porous high internal surface area anodes for highly efficient oxygen evolution reaction (OER) during water splitting reactions. Thus, these earth abundant mixed transition metal oxide anodes can be coupled with active metal or mixed metal cathodes to develop solar cell powered electrolyzers for efficient generation of oxygen and hydrogen fuel by water splitting.

References


