

This paper is part of the Proceedings of the 14th International Conference on Simulation and Experiments in Heat Transfer and its Applications (HT 2016) VFERENCES www.witconferences.com

Turbulent Rayleigh–Bénard convection scaling in a vertical channel using the lattice Boltzmann method

Y. Wei & H. Dou

Faculty of Mechanical Engineering and Automation, Zhejiang Sci-Tech University, China

Abstract

The existing scaling laws for turbulent Rayleigh-Bénard convection of air in a differentially heated vertical channel is investigated via the lattice Boltzmann method (LBM). Based on the arguments of an inner (near-wall) and outer (channel centre) region, the simulation results are found to support a minus onethird power law for the mean temperature in an overlap region. Using the inner and outer temperature profiles, an implicit heat transfer equation is shown. A correction term is non-negligible for the present Ra range when compared with the explicit equations found in this paper. Finally, it is shown that the results of present LBM about the Nusselt number Nu as a function of Rayleigh number are in good agreement with the theoretical values.

Keywords: turbulent, Rayleigh–Bénard convection, scaling, LBM.

1 Introduction

The heat transfer in a channel has been widely studied in some thermal engineering applications such as solar thermal receivers. One of the prevalent industry practices is to control the heat gain or loss of the building by insulating the external building envelope. The key to a deeper understanding of the mechanisms of heat and momentum in turbulent Rayleigh-Bénard convection lies in better access to the dynamic in the scaling of temperature and velocity of an inner (near-bottom wall) and outer (channel centre) region [1]. The Reynoldsaveraged Navier-Stokes simulations (RANS) and the large eddy simulations (LES) are important to have accurate wall models, especially since these models set the boundary conditions for calculations close to the wall [2]. The added



computational cost associated with fine grid spacing, a requirement for capturing rapid changes in flow physics near the wall are reduced. As such, it is important to have accurate wall models that are valid for a large range of flow conditions. Rayleigh–Bénard convection, as a typical benchmark problem, has been received noticeable attention from the lattice Boltzmann method (LBM) community owing to its geometric simplicity and its complex flow features at different Rayleigh numbers. Although most of studies just concentrate on the laminar and transitional Rayleigh–Bénard convection [3, 4].

Hölling and Herwig and Shiri and George have developed wall functions using various scaling analyses (e.g. [5–8]). However, the opinions of these studies have largely been found to differ, possibly due to the limited numerical data at the time. The existing scaling laws for turbulent Rayleigh–Bénard convection of air in a differentially heated vertical channel are studied in this paper. Based on the arguments of an inner (near-wall) and outer (channel centre) region, the results of simulation are found to support a minus one-third power law for the mean temperature in an overlap region. Using the inner and outer temperature profiles, an implicit heat transfer equation is shown. In the following, a simple lattice Boltzmann thermal model will be briefly described at first. Then the problem definition and numerical verification are followed. A fter that, the detailed discussions of turbulence Rayleigh–Bénard convection scaling are investigated. Finally, some concluding remarks are provided.

2 Numerical method

The numerical algorithm used is based on the discrete kinetic models. The starting point is a standard coupled mesoscopic dynamics described by [4]:

$$f_i(x+c_i\Delta t,t+\Delta t) = f_i(x,t) + \left[f_i^{eq}(x,t) - f_i(x,t)\right] / \tau_v + F_i \quad (1)$$

$$g_i(x+c_i\Delta t,t+\Delta t) = g_i(x,t) + \left[g_i^{eq}(x,t) - g_i(x,t)\right] / \tau_T$$
(2)

where $f_i(x,t)$, $g_i(x,t)$ stand for the probability density functions to find at (x,t) a particle velocity belongs to a discrete and limited set C_i (with $i = 0, 1, 2, \dots 18$ in the D3Q19 LBM adopted here [3]). F_i is the momentum input from the buoyant body force, τ_v and τ_T are the relaxation time for flow and temperature LB equations. The additional buoyant body force term F_i can be formulated by the Boussinesq approximation, i.e.

$$F_i = 3w_i \cdot \rho \cdot \mathbf{g} \cdot \beta \cdot T \cdot c_{iv} \tag{3}$$

where **g** is the acceleration of gravity, β is the thermal expansion coefficient, c_{iv} is the y-component of $C_i \cdot f_i^{eq}$ is a single-particle equilibrium distribution



function which is derived from a Maxwell-Boltzmann distribution and can be approximated to

$$f_{i}^{eq} = \rho w_{i} \left[1 + \frac{c_{i} \cdot u}{c_{s}^{2}} + \frac{(c_{i} \cdot u)^{2}}{c_{s}^{2}} - \frac{u^{2}}{2c_{s}^{2}}\right] \cdot g_{i}^{eq} = w_{i} T \left[1 + \frac{(c_{i} \cdot u)}{c_{s}^{2}}\right]$$
(4)

For a D3Q19 lattice, shown in Figure 1, we have:



Figure 1: Lattice velocity directions in D3Q19 lattice structures [3].



Figure 2: Schematic diagram of RB convection in a vertical channel.

A Chapman–Enskog expansion leads to the equations (5)–(7) for the density, momentum, and temperature equation based on equations (1) and (2). The streaming step on the left-hand side reproduces the inertial terms in the hydrodynamical equations, whereas dissipation and thermal diffusion are

connected to the relaxation (towards equilibrium) properties in the right hand side, with τ_v and τ_T related to the relaxation times.

$$\frac{\partial \rho}{\partial t} + \nabla \cdot (\rho \mathbf{u}) = 0 \tag{5}$$

$$\frac{\partial(\rho \mathbf{u})}{\partial t} + \nabla \cdot (\rho \mathbf{u} \mathbf{u}) = -\nabla p + \nabla \cdot (2\rho v \mathbf{S}) - g\beta \Delta T$$
(6)

$$\frac{\partial T}{\partial t} + \mathbf{u} \cdot \nabla T = \Gamma \nabla^2 T \tag{7}$$

3 Numerical simulations and discussions

A computational domain size is defined by $L_x \times L_y \times L_z$ with the resolutions $M_x \times M_y \times M_z = 456 \times 228 \times 228$ for $Ra = 6.0 \times 10^6$, and $M_x \times M_y \times M_z = 656 \times 328 \times 328$ for $Ra = 4.0 \times 10^7$. The side boundaries of the channel were assigned periodic boundary conditions for both the flow and temperature fields. Meanwhile, the upper and bottom solid boundaries were assigned no-slip conditions for the flow field and were assigned non-dimensional temperatures of $T_{up} = 0$ and $T_{down} = 1$.

Figure 3 presents snapshots of the isosurfaces of the temperature fields. The red is hot plumes and the blue is cold plumes. By integrating the Eq. (7), we obtain

$$\Gamma \frac{\partial T}{\partial z} - u_z T = -\frac{q_z}{\rho C_p} = Q_z \tag{8}$$

which describes a characteristic heat flux constant_{$Q_z} equivalent$ to the wall heat flux q_z flowing from left to right divided by density ρ and specific heat C_p . The outer temperature scale depends on the channel half-high *h*, the inner and outer temperature scales are:</sub>

$$T_{i} = \left(\frac{|Q_{z}|^{3}}{g\beta\Gamma}\right)^{1/4}, T_{o} = \left(\frac{|Q_{z}|^{2}}{g\beta h}\right)^{1/3}$$
(9)

The respective inner and outer length scales are defined as:

$$l_i = \left(\frac{\Gamma^3}{g\beta|q_z|}\right)^{1/4} \text{ and } l_o = h$$
(10)

To use the above scaling and the gradient-matching approach, the following power-law forms of the temperature wall functions are obtained [7].

$$\frac{T_{h} - \bar{T}}{T_{i}} = -c_{1} \left(\frac{z}{l_{i}}\right)^{-1/3} - c_{2} (\text{Pr}), \text{ and } \frac{\bar{T} - T_{ref}}{T_{o}} = c_{1} \left(\frac{z}{l_{i}}\right)^{-1/3} - c_{3}$$
(11)





Figure 3: Snapshots of instantaneous isotherms with $M_y = L_y/2$ at $Ra = 4.0 \times 10^7$.

The constants to be: $c_1 = 4.2$ and $c_2 = -5$ are obtained in the study by Versteegh and Nieuwstadt (1999).

In this paper, a new inner temperature wall function with fitted constants is used:

$$\frac{T_h - \bar{T}}{T_i} = -4.2 \left(\frac{z}{l_i}\right)^{-1/3} + 5.0$$
(12)

Figure 4 shows that temperature data plotted in inner and outer scaling with evidence of adherence to power-law behavior with two *Rayleigh* numbers. It is found that the LBM results are in good agreement with the present theoretical values. To appraise these wall functions, we qualitatively assess their respective fits to the present data of LBM in both inner and outer scales, shown in Figure 4(a) and (b).

The analysis of the mean heat transport is represented by the *Nusselt* number in the following section. Firstly we discuss the relations of the turbulent heat flux in their dimensionless form, the *Nusselt* number $Nu = 1 + \langle u_z T \rangle / (\Gamma \Delta T / H)$ and the *Rayleigh* number is $Ra = (\beta \Delta TgH^3) / (vT)$. It is shown that the *Nusselt* number *Nu* is as a function of *Rayleigh* number. A clear scaling can be seen for *Nu* (*Ra*) for $Ra \approx 10^5$ to 10^8 . The theoretical values in Figure 5 is presented by the

following equation $Nu \sim Ra^{0.291}$.

Figure 5 displays that the blue dots are the results of present LBM, the black squares represent the simulation results of DNS study by Kaczorowski and Wagner [9], and the red line represents the theoretical values [9]. It can be seen clearly that the results of present LBM are better agreement with the theoretical values than the results of DNS. In addition, it is shown that the results of present LBM about the *Nusselt* number *Nu* as a function of *Rayleigh* number are in good agreement with the theoretical values.







W



Figure 5: The *Nusselt* number *Nu* as a function of *Rayleigh* number.

4 Conclusion

We show evidence that provide additional support for a minus one-third power law for the mean inner and outer temperature wall function in an overlap region from the present LBM dataset for $Ra = 6.0 \times 10^6$ and $Ra = 4.0 \times 10^7$. Using the inner and outer temperature profiles, an implicit heat transfer equation is shown. In addition, it is shown that the results of present LBM are better agreement with the experimental results than the results of DNS about the *Nusselt* number *Nu* as a function of *Rayleigh* number. Finally, it is shown that the results of present LBM about the *Nusselt* number *Nu* as a function of *Rayleigh* number are in good agree with the theoretical vales.

Acknowledgement

This work is supported by the Science Foundation of Zhejiang Sci-Tech University under Grant No 1130032611308.

References

- N. Azwadi, A.R.M. Rosdzimin, Simulation of natural convection heat transfer in an enclosure using lattice Boltzmann method, J Mekanikal, 2008, 27, 42–50.
- [2] M.A. Mussa, S. Abdullah, C.S. Nor Azwadi, N. Muhamad, Simulation of natural convection heat transfer in an enclosure by the lattice-Boltzmann method, Computers & Fluids, 2011, 44, 162–168.



- [3] Y.H. Qian, D. d'Humieres, P. Lallemand, Lattice BGK models for Navier– Stokes equation, Europhys Lett, 1992, 17(6), 479–484.
- [4] P.H. Kao, R.J. Yang, Simulating oscillatory flows in Rayleigh–Bénard convection using the lattice Boltzmann method, Int J Heat Mass Transfer, 2007, 50, 3315–3328.
- [5] C.K. Aidun, Lattice-Boltzmann method for complex flows, Annual Review of Fluid Mechanics, 2010, 42, 439–472.
- [6] R.D. Moser, J. Kim, N.N. Mansour, Direct numerical simulation of turbulent channel flow up to Res = 590, Phys Fluids, 1999, 11, 943–945.
- [7] J. Pallares, A. Vernet, Turbulent large-scale structures in natural convection vertical channel flow, Int J Heat Mass Transfer, 2010, 53, 4168–4175.
- [8] A. Shiri, W.K. George, Turbulent natural convection in a differentially heated vertical channel. In: Proceedings of 2008 ASME Summer Heat Transfer Conference.
- [9] M. Kaczorowski, C. Wagner, Analysis of the thermal plumes in turbulent Rayleigh–Bénard convection based on well resolved numerical simulations, Journal of Fluid Mechanics, 2009, 618, 89–112.

