Experimental study of toluene decomposition by combination of barrier discharge plasma and UV light

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Abstract

The combination of dielectric barrier discharge plasma (DBD) and ultraviolet irradiation (UV) on the decomposition of toluene was studied.

The decomposition rate of toluene by combination of DBD and UV, as well as reaction products were studied in a 0.5 m³ stainless steel closed chamber. The synergetic effect was found in toluene decomposition by combination of DBD and UV. This parameter increases sharply in comparison to the decomposition rate of toluene by both DBD and UV separately.

Ion cluster concentration was also increased whereas ozone accumulation concentration was dramatically decreased.

An obtained phenomenon was discussed due to the difference of oxidation rates between ozone and hydroxyl radicals which are produced by the decomposition of ozone by UV light.

Keywords: plasma, toluene decomposition, UV light, ozone, ion cluster.

1 Introduction

Plasma air treatment is a subject of many investigations to use it for indoor air pollution control [1-4]. The main advantage of it is a decomposition of gaseous air pollutants at room temperature. The decomposition rate of air pollutants is mainly depended on a discharge voltage. The higher discharge voltage the higher decomposition rate.

At the same time a decomposition rate of contaminants by plasma treatment accompanied to the formation of minor amount of harmful by-products such as



ozone, carbon monoxide, and aerosol particles [5, 6]. The quantity of them also depends on discharge voltage or supplied energy into plasma. The higher supplied energy the higher the amount of by-products.

In order to overcome this duality the researchers [7, 8] paid their attentions to develop combination systems based on plasma treatment and other additional methods like catalyst [7], water scrubber [8].

In the study [9] was shown that the utilization of ozone catalyst coated onto the fan wheel in plasma air cleaner allowed the discharge voltage to be increased up to 20% without changing an ozone concentration in outlet of air cleaner.

Combination of dielectric barrier discharge plasma (DBD) and ultraviolet irradiation (UV), hereafter named as DBDUV on the decomposition of toluene was experimentally studied. The decomposition of toluene by (DBD) as well as by UV was also studied for comparison.

2 Experimental

2.1 Reaction chamber

A closed stainless steel chamber (0.5 m³) was used in this experiment, fig. 1. Inside of a chamber was placed air cleaner system consisting of dielectric barrier discharge device and ultraviolet lamp, fig. 1. The DBD device was the glass tube coated inside with a silver film as a high voltage electrode and a stainless steel net covering the glass as a ground one. The high voltage 60 Hz frequency AC power supply was used for formation of barrier discharge plasma in surrounding of glass tubes. The ultraviolet lamp was Hg-lamp "PL-L 18W" (Philips).

Gaseous toluene was prepared by bubbling toluene liquid with air at 285 K and injected into chamber to form a known initial concentration of toluene. Contents of the chamber were mixed by fan with 60 CMH, continuously.

2.2 Analyses

The alteration of toluene concentration in the chamber during reaction time was controlled by "PGM-7420", CO and CO_2 by "PGM-5210" IAQRAE Rae analyzers (USA) and Gastec glass tube (Japan), and ozone concentration by "49C ozone calibrator" (USA) and Gastec glass tube.

Accumulation of ion produced by DBD, UV, and DBDUV were controlled by ion meter "T-111" Transjionic AB (Sweden).

The decomposition rate (DR) of toluene was determined by:

$$DR = \frac{([C_7H_8]_0 - [C_7H_8]_I}{[C_7H_8]_I}$$
(1)

where $[C_7H_8]_0$ and $[C_7H_8]_I$ are the initial and the current toluene concentrations, respectively.



Oxidation rate of toluene was described as a parameter (S) which is defined by:

$$S = \frac{([CO_2]_I - [CO_2]_O) + [CO_I]}{([C_7H_8]_O - [C_7H_8]_I)^*7}$$
(2)

where $[CO_1]$, $[CO_2]_I$ and $[CO_2]_O$ are the current and the initial carbon monoxide, carbon dioxide concentrations, respectively; $[C_7H_8]_O$ and $[C_7H_8]_I$ are the initial and the current toluene concentrations, respectively.



Figure 1: Experimental system for toluene decomposition: 1- Fan. 2 – DBD device; 3 – UV lamp; 4 – High voltage transformer; 5 – Stainless steel chamber.

3 Results

3.1 Efficiency improvement by UV irradiation

In order to improve DBD method for removal of indoor VOCs, the decomposition of toluene was studied in the presence of UV. In fig. 2 are shown the decomposition of toluene by three methods: DBD, UV, and DBDUV. High voltage supplied to barrier discharge tube was 2.8 kV. The decomposition rates of toluene by DBD as well as UV irradiation are nearly the same. Maximum decomposition rate is not higher than 7.5% for both cases for 2 hours. However, this value is dramatically increased by using DBDUV. The decomposition rate of toluene is increased up to 30% for the same time. This value is almost two times more than the sum of decomposition rate of toluene obtained by DBD and UV



when they used separately. It means some synergetic effect is present in this case.



Figure 2: Toluene decomposition rate in metal chamber (0.5 m^3) by DBD (B), UV (C) and DBDUV. Discharge voltage was 2.8kV: Initial concentration (C₀) of toluene were: (C₀)_B = 3.48 ppm; (C₀)_C = 2.54ppm; (C₀)_D = 3.52 ppm.

It is well known an ozone formation is a main problem by utilizing DBD for air pollution control because it is strongly regulated by the occupational safety health administration.



Figure 3: Ozone accumulation in metal chamber (0.5 m³) by UV (B), by DBD (C), and DBDUV (D). Discharge voltage was 2.8 kV.

In fig. 3 are shown the ozone accumulation concentrations which measured during toluene decomposition by three methods: DBD, UV, and DBDUV.

The accumulation concentration of ozone was significantly lower during toluene decomposition by DBDUV in comparison with DBD. It was 0.5 ppm for

2 hour only whereas ozone accumulation concentration for DBD was 2.0 ppm for the same time. Ozone concentration was not practically changed during toluene decomposition by UV.

Ion clusters forming during DBD operation is one of parameters indicating the quality of air cleaner because they play important role in the indoor environment [7]. The higher the concentration of ion clusters the higher quality of the air cleaner. In fig. 4 are shown the ion concentrations accumulated in the blank metal chamber by operation of DBD, UV, and DBDUV.



Figure 4: Ion accumulation in blank metallic chamber (0.5 m³) by UV (B), DBD (C), DBDUV (D). Discharge voltage was 2.8 kV.

The data indicates the ion concentration was at the level of 4000 ion cm^{-3} for 60 second by DBDUV whereas for other two methods was 1000 ion cm^{-3} for the same time only.

The other parameter which must be controlled by application of BDP for indoor air cleaning is oxidation rate (S) of toluene because the uncompleted oxidation products like aldehydes, organic acids, etc can be formed. The higher oxidation rate the higher the quality of air cleaner.

Obtained data indicate the oxidation rate of toluene by two methods has complicated character. It will be discussed below.

3.2 Influence of initial concentration of toluene

Synergetic effect for toluene decomposition by DBDUV is kept at increasing the initial concentration of toluene. As seen from figure 5 the decomposition rate of toluene by DBDUV is much higher than that of DBD. Moreover the difference between two decomposition rates is as much more as higher the initial concentration of toluene. The difference between two methods was 3.5 ppm at initial concentration of around 16 ppm whereas its value was 1.5 ppm only for initial concentration of around 3 ppm.

As for the decomposition rate of toluene in dependence of initial concentration, it is decreased with increasing toluene concentration. However, it



is necessary to note the total toluene molecules decomposed increases with increasing toluene concentration, fig. 6.



Figure 5: Toluene decomposition in metal chamber (0.5 m³) by DBDUV (B, E) and DBD (C, D) at different concentration. Discharge voltage was 3.8 kV. Initial concentration (C₀) in ppm were: $C_0(B) = 16.5$; $C_0(C) = 12.0$; $C_0(D) = 3.61$; $C_0(E) = 3.0$.



Figure 6: Toluene decomposition in metal chamber (0.5 m³) by DBDUV with varied initial concentrations of toluene. Discharge voltage was 3.8 kV. Initial concentrations were B – 29.3 ppm; C – 17.5 ppm; D – 7.2ppm.

3.3 Influence of discharge voltage

Discharge voltage is very important parameter for DBD because it regulates both the decomposition rate of air pollutants and the formation of by products like CO, uncompleted oxidation compounds, and O_3 .





Figure 7: Toluene decomposition rate in metallic chamber (0.5m³) by DBDUV at varied discharge voltages: B – 2.8 kV; C – 3.4 kV; D – 3.8 kV. Initial concentration of (B) = 3.48 ppm; (C) = 2.54 ppm; (D) = 3.52 ppm.

In fig. 7 are shown the decomposition rates of toluene by DBDUV at three discharge voltages: 2.8, 3.4, and 3.8 kV. They indicate the higher discharge voltage the higher the decomposition rate of toluene.

In table 1 is shown data about toluene decompositions by DBD and DBDUV.

Table 1:Toluene abatement rates (%) by BDP, UV irradiation, and
combination of BDP and UV at varied discharge voltages.
Treatment time was 120 min.

High voltage,	DBD	DBDUV	DBDUV-DBD	
kV				
2.8	7.5	30	22.5	
3.4	10.6	50	31.9	
3.8	12.5	77	64.5	

The tendency of synergetic effect for the decomposition of toluene by DBDUV is kept at varied discharge voltages too. Moreover, this effect for toluene decomposition is as much higher as the higher discharge voltage.

The difference of toluene decomposition rate between DBDUV and DBD (DBDUV-DBD) was 64.5% at 3.8 kV whereas it was 22.5% at 2.8 kV only.

4 Discussion

Synergetic effect for the decomposition of toluene by DBDUV is a very interesting and potentially useful phenomenon. In order to explain this phenomenon it is necessary to understand toluene oxidation mechanism by DBD as well as UV.



Sekiguchi *et al.* [10] investigated the toluene hydroxylation by DBD plasma. They considered two types of oxygen atoms are responsible for toluene oxidation:

$O(^{3}P)$ – an atomic oxygen in the ground state;

$O(^{1}D)$ – an exited oxygen atom created by impact with O_{2} .

The $O(^{1}D)$ is the strong oxidant for toluene to produce oxidation product such as CO and OH by breaking the aromatic structure whereas the $O(^{3}P)$ is a effective reagent for partial oxidation [10].

On other hand, Atkinson and Carter [11] showed OH radical is key reactive specie for most organics. The most organics react with the OH radical with rate constants of $\ge 5 \times 10^{-15}$ cm³ molecule s⁻¹ at 298 K whereas an ozone reacts with toluene at the reaction rate constant of $1.2\pm0.6 \times 10^{-20}$ cm³ molecule s⁻¹ at 298 K [11]. Influence of UV irradiation on the toluene oxidation was investigated by Wang and Ray [12]. They postulated the main species for toluene oxidation are also OH radical and O(¹D) which can be occured by:

$$H_2O + hv = H^{\bullet} + OH^{\bullet}.$$
 (3)

$$H_2O + hv = H_2 + O(^{3}P) \text{ or } O(^{1}D)$$
 (4)

According to this review, synergetic effect obtained at a toluene decomposition by DBDUV is associated with the formation of additional amount of hydroxyl radical which can be formed from ozone due to [11]:

$$O_3 + hv (\lambda \le 310 \text{ nm}) = O(^1D) + O_2(^1\Delta_g)$$
 (5)

$$O(^{1}D) + H_{2}O = 2OH^{\bullet}$$
(6)

Maybe it confirms indirectly by that the ozone accumulation is dramatically decreased by DBDUV in comparison by DBD, fig. 3, at constant ozone production rate which was 0.048 ml/min at discharge voltage 2.8 kV. These differences between two methods are as much higher as higher discharge voltage in the range of 2.8 to 3.8 kV, table 2.

Table 2: Ozone accumulation (ppm) in metal chamber during toluene decomposition by DBD, UV, and DBDUV. Treatment time was 120 min.

High voltage, kV	DBD	UV irradiation	DBDUV
2.8	2.07	0.02	0.67
3.4	3.95	0.02	1.56
3.8	5.20	0.02	2.06



In table 3 are shown the parameters (S) indicating the accumulation of CO and CO₂ during toluene decomposition. $\blacktriangle C_{C7H8}$ is the decomposed toluene concentration and $\blacktriangle C_{C02}$ as well as $\blacktriangle C_{C0}$ are carbon dioxide and carbon monoxide concentrations, respectively.

DV	UV	▲C _{C7H}	▲C _{CO} ,	▲ C _{CO2} ,	▲C _{CO} ,	▲C _{CO2} ,	S	S
kV	lig	8	ppm,	ppm,	ppm,	ppm,	by	by
	ht	ppm	by	by	by	by	gas	RA
			gastec	gastec	RAE	RAE	tec	Ε
2.8	no	10	5	70	2	-150	1.1	-
								2.1
2.8	yes	12.1	10	-100	4	100	-	1.2
	-						1.1	
3.4	no	15	10	100	9	-40	1.0	-
								0.3
3.4	yes	16.3	15	0	13	70	0.1	0.7
3.8	no	23	20	100	9	-80	0.8	-
								0.4
3.8	yes	25.4	30	100	23	150	0.7	1.0

Table 3:Selectivity to CO2 and CO for toluene oxidation by two methods:
plasma and combination of plasma and UV irradiation.

The parameters (S) defined on the base of CO_2 and CO measurements by Gastec and RAE devices are quite different. Moreover some values of them has negative one. It could be explained by formation of different by-products at different reaction conditions influencing on the readings of CO_2 . It could be the products of partial oxidation of toluene. Our attempt to segregate these by-products was not successful. According to [10] the by-products of partial oxidation of toluene were C_4 - compounds such as butadiene and other hydrocarbons which were also not identified completely.

On other hand, it indicates the oxidation rate of toluene depends on the discharge voltage of DBD plasma and can be controlled by variation of this parameter. It will be a next subject of further study.

5 Conclusions

The decomposition of toluene by DBD plasma as well as the combination of DBD and UV irradiation was carried out in closed metal chamber. The experimental data suggested that the synergetic effect were occurred both in the decomposition of toluene and decreasing ozone accumulation in the reaction region by means of combination of DBD and UV. The decomposition rate of toluene was dramatically increased whereas ozone concentration decreased significantly in comparison with DBD.



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